Interfacial Tension of Hydrocarbon + Water/Brine Systems under High Pressure

Bi-Yu Cai, Ji-Tao Yang, and Tian-Min Guo*

High Pressure Fluid Phase Behavior & Property Research Laboratory, University of Petroleum, Beijing 100083, P. R. China

Interfacial tensions of 10 normal alkane + water/brine and hydrocarbon mixture + water/brine systems were measured by using a pendent drop instrument. The temperature and pressure ranges of measurements are (25 to 80) °C and (1 to 300) bar, respectively. The effects of temperature, pressure, and salt content have been studied. It was found that the interfacial tension is sensitive to temperature and salt concentration but weakly dependent on pressure and salt species.

Introduction

The interfacial tension of hydrocarbon + water/brine systems is one of the basic physical properties required for performing process calculations in petroleum, natural gas, and petrochemical industries. Although numerous surface/ interfacial tension data under normal pressure and temperature have been reported in the literature (Nakahara and Masamoto, 1990; Sada et al., 1975), only a few data under high pressures and elevated temperatures were reported (Matubayasi et al., 1977; McCaffery, 1972; Jennings, 1967), and inconsistent pressure effects were observed.

There are few high-pressure interfacial tension measurements on hydrocarbon + brine systems.

For developing a generalized interfacial tension model capable of applying to reservoir engineering and other highpressure applications, sufficient basic data are required. In this work, the interfacial tension of six pure liquid *n*-alkanes and four hydrocarbon mixtures with water/brine have been measured in the pressure range of (1 to 300) bar and temperature range of (25 to 80) °C. The effects of pressure, temperature, molecular weight of hydrocarbons, and salt species and concentration have been examined.

Experimental Section

Reagents. The purity and the source of chemicals used are listed in Table 1. Distilled water was deionized by a Model 70 ion-exchanger manufactured by Nan-Hua Medical Apparatus Corp. (China). The salt content of the seven brines prepared are given in Table 2.

Apparatus and Procedure. The JEFRI pendent drop high-pressure interfacial tension apparatus manufactured by DB Robinson Ltd. (Canada) was used in this work. The schematic flow diagram of the experimental system and the cross-sectional view of the pendent drop cell are shown in Figures 1 and 2, respectively. The maximum working range of the apparatus is 345 bar and 200 °C. The precision of measurements are as follows: pressure $\pm 0.25\%$, temperature ± 0.25 °C, drop dimension ± 0.01 mm. The accuracy of the calculated interfacial tension is estimated to be ± 0.05 mN·m⁻¹.

The standard procedure used in the pendent drop method was followed, and the detailed description of the experimental procedure is given elsewhere (Cai, 1995). For checking the reliability of the apparatus and procedure applied, the interfacial tension of benzene + water was measured at 1.013 bar and 30.0 °C; the measured value



Figure 1. Schematic flow diagram of the pendent drop interfacial tension experimental system: (1) vibration-free bench; (2) sample cylinder; (3) pendent drop cell; (4) vacuum pump; (5) pressure gauge; (6) hand pump.

Table 1. Reagents Used in This Work

reagent	grade	conc/mass %	source
<i>n</i> -alkanes	analytical	99.0	Sigma Corp.
sodium	analytical	99.5	Tang-Gu Chemical
chloride			Reagents, Tianjin
magnesium	analytical	$\geq \! 98.0$	Double-Ring
chloride	U		Chemical Reagents,
			Beijing
calcium	analytical	98.0	Tian-Ýan Fine
chloride	·		Chemicals, Tianjin

Table 2. Salt Content and Ionic Strength in Various Brines (t = 25 °C, P = 1.013 bar)

brine no.	salt species	salt concn/mol/L	ionic strength/mol/L
1	NaCl	0.8847	0.8847
2	$NaCl + CaCl_2$		1.1390
	-NaCl	0.4400	0.4400
	$-CaCl_2$	0.2330	0.6990
3	NaCl	0.0854	0.0854
4	NaCl	0.1716	0.1716
5	NaCl	1.8069	1.8069
6	MgCl ₂	0.5301	1.5903
7	CaCl ₂	0.4650	1.3950

 $(33.2 \text{ mN} \cdot \text{m}^{-1})$ is in close agreement with the value of 33.0 mN·m⁻¹ reported by Jennings (1967).

Results and Discussion. The interfacial tensions of six normal alkanes (hexane, octane, decane, dodecane, tetradecane, and hexadecane) with pure water and brines were measured at 25.0 and 50.0 °C under various pressures, and the results are listed in Table 3. Similar results for three ($C_6 + C_{10}$) binary mixtures and one ($C_6 + C_{10} + C_{10}$)

© 1996 American Chemical Society

Table 3. Interfacial Tensions of Alkane + Water/Brine Systems

a. Interfacial Tension of *n*-Alkane + Water/Brine 1/Brine 2 Systems

]	H ₂ O	br	rine 1		brine 2]	H ₂ O	br	rine 1	bı	rine 2
<i>n</i> -		<i>P</i> /	σ/	<i>P</i> /	σ/	<i>P</i> /	σ	<i>n</i> -		<i>P</i> /	σ/	<i>P</i> /	σ/	<i>P</i> /	σ/
alkane	t/°C	bar	$mN \cdot m^{-1}$	bar	$mN \cdot m^{-1}$	bar	mN⋅m ⁻¹ ms	alkane	t/°C	bar	$mN \cdot m^{-1}$	bar	$mN \cdot m^{-1}$	bar	$mN \cdot m^{-1}$
C ₆	25.0	36.9	50.73	36.9	53.16	38.7	53.21	C ₁₂	25.0	36.9	51.97	40.4	54.18		
		109.0	50.97	109.0	53.41	109.0	53.44			105.6	52.45	109.0	54.40		
		162.2	51.18	162.2	53.65	153.6	53.83			160.5	52.79	165.6	54.37		
		215.3	51.38	220.5	53.92	220.5	54.00			215.3	53.03	225.6	55.09		
		289.1	51.71	292.5	54.16	282.2	54.24			284.0	53.31	289.1	52.85		
	50.0	40.4	48.04	38.7	50.26	43.1	50.55		50.0	40.4	49.50	38.7	51.54		
		115.9	48.22	115.9	50.54	107.3	50.79			105.6	49.69	109.0	51.79		
		165.6	48.46	165.6	50.74	157.0	51.24			162.2	49.97	158.7	52.06		
		211.9	48.80	211.9	51.97	218.8	51.38			222.2	50.30	218.8	52.43		
		290.8	48.95	289.1	51.29	289.1	51.67			284.0	50.74	289.1	52.85		
C_8	25.0	40.4	51.04	38.7	53.50			C ₁₄	25.0	38.7	52.48	40.4	54.62		
		109.0	51.38	109.0	53.72					112.4	52.68	109.0	54.96		
		155.3	51.66	155.3	54.13					160.5	53.05	163.9	55.28		
		215.3	51.91	213.5	54.30					223.9	53.40	217.1	55.60		
		284.0	52.13	284.0	54.55					285.7	53.78	285.7	55.97		
	50.0	40.4	48.33	38.7	50.88				50.0	36.9	49.99	38.7	51.99		
		110.7	48.50	105.6	51.14					110.7	50.28	110.7	52.39		
		153.6	48.83	148.4	51.33					158.7	50.77	155.3	52.88		
		223.9	49.12	220.5	51.69					220.5	50.95	217.1	53.04		
		289.1	49.30	282.2	51.99					290.8	51.29	292.5	53.32		
C ₁₀	25.0	43.1	51.51	40.4	53.74	38.7	53.78	C ₁₆	25.0	36.9	52.91	36.9	55.05	36.9	55.07
		105.6	51.84	103.8	53.97	110.7	54.04			105.6	53.21	107.3	55.45	105.6	55.48
		160.5	52.10	155.3	54.17	160.5	54.15			162.6	53.49	158.7	55.82	150.2	55.78
		213.5	52.41	218.8	54.58	215.3	54.62			225.6	53.93	220.5	56.14	218.8	55.97
		282.2	52.65	284.0	54.82	284.0	54.93			292.5	54.26	282.2	56.46	289.1	56.43
	50.0	38.7	49.00	38.7	51.06	40.4	51.20		50.0	36.9	50.31	43.1	52.78	43.1	52.73
		98.7	49.31	112.4	51.27	105.6	51.52			110.7	50.93	110.7	53.01	105.6	53.02
		157.0	49.55	155.3	51.61	162.2	51.79			158.7	51.14	157.0	53.35	150.2	53.32
		210.2	49.84	223.9	51.88	222.2	52.00			222.2	51.37	223.9	53.68	220.5	53.72
		278.8	50.05	289.1	52.33	284.0	52.23			284.0	51.88	282.2	54.12	285.7	54.14

b. Interfacial Tension of Octane + Brine (Brine 3 to Brine 7) Systems at 25 $^\circ\mathrm{C}$

b	rine 3		orine 4	b	brine 5		brine 6		orine 7
P/bar	$\sigma/\mathbf{mN}\cdot\mathbf{m}^{-1}$	P/bar	$\sigma/\mathbf{mN}\cdot\mathbf{m}^{-1}$	P/bar	$\sigma/\mathbf{mN}\cdot\mathbf{m}^{-1}$	P/bar	$\sigma/mN \cdot m^{-1}$	P/bar	$\sigma/mN\cdot m^{-1}$
40.4	51.88	42.1	52.73	40.4	56.11	40.4	53.60	38.7	53.69
110.7	52.01	107.3	53.04	109.0	56.31	109.0	53.79	109.0	54.07
155.3	52.23	151.9	53.43	155.3	56.54	153.6	54.08	160.5	54.29
218.8	52.45	215.3	53.70	213.5	56.84	211.9	54.49	215.3	54.43
289.1	52.81	284.0	53.94	284.0	57.10	278.8	54.67	280.5	54.68

 $C_{16})$ ternary mixture are tabulated in Table 4. The compositions (mole fraction) of the hydrocarbon mixtures studied were

hexane (1) + decane (2):
$$x_1 = 0.3734$$
; $x_1 = 0.5978$;
 $x_1 = 0.7825$

hexane (1) + decane (2) + hexadecane (3): $x_1 = 0.4293$, $x_2 = 0.2518$

Typical pressure effects on the interfacial tension are shown in Figures 3 and 4. Since the interfacial tension is weakly dependent on pressure and increases almost linearly with pressure, the measured isothermal interfacial tensions were smoothed by the following correlation:

$$\sigma = \alpha + \gamma P \tag{1}$$

where σ stands for the interfacial tension at absolute pressure *P*, α is a constant, and γ is a pressure coefficient $(\partial\sigma/\partial P)_T$. The regressed α and γ values for the 20 hydrocarbon + water/brine systems are given in Table 5.

The comparisons of the calculated, based on eq 1, and the reported literature values for four *n*-alkane + water systems at 25 °C (20 data points) are presented in Table 6. The absolute average deviation is $0.25 \text{ mN} \cdot \text{m}^{-1}$, and the deviation slightly increases with pressure.



Figure 2. Cross-sectional view of the high-pressure pendent drop cell: (1) capillary tube; (2) view window; (3) sealing ring; (4) window cover; (5) main body; (6) exit tube.

 Table 4. Interfacial Tension of Hydrocarbon Mixture + Water/Brine Systems

		H ₂ O		b	orine 1	brine 2		
hydrocarbon mixture	t/°C	P/bar	$\sigma/mN \cdot m^{-1}$	P/bar	$\sigma/mN \cdot m^{-1}$	P/bar	$\sigma/mN \cdot m^{-1}$	
hexane (1) + decane (2)	25.0	43.1	51.35	40.4	53.59	38.7	53.63	
$x_1 = 0.3734$		102.1	51.53	103.8	53.98	95.7	54.00	
$x_2 = 0.6266$		148.4	51.78	151.9	54.30	160.5	54.31	
		217.5	52.04	215.3	54.54	217.6	54.60	
		285.7	52.37	290.8	54.89	287.4	54.92	
	50.0	38.7	48.30	38.7	50.99	40.4	51.04	
		102.1	48.60	109.0	51.14	110.7	51.33	
		151.9	48.85	155.3	51.45	148.4	51.74	
		217.1	49.07	213.5	51.76	223.9	51.89	
		278.8	49.40	284.0	52.07	285.7	52.15	
hexane (1) + decane (2)	25.0	40.4	50.94	42.1	53.50	38.7	53.60	
$x_1 = 0.5978$		103.5	51.25	102.1	53.73	102.1	53.81	
$x_2 = 0.4022$		160.5	51.57	144.8	54.05	155.3	54.06	
		227.4	51.81	215.3	54.35	225.6	54.34	
		280.5	52.06	280.5	54.77	285.7	54.67	
	50.0	42.1	48.23	43.1	50.79	42.1	50.92	
		110.7	48.73	107.3	51.06	102.1	51.17	
		155.3	49.00	153.6	51.36	150.2	51.44	
		223.9	49.28	215.3	51.70	222.2	51.74	
		287.4	49.54	287.4	52.02	282.2	52.07	
hexane (1) + decane (2)	25.0	40.4	50.74	42.1	53.34	43.1	53.35	
$x_1 = 0.7825$		109.0	50.98	99.1	53.54	105.6	53.71	
$x_2 = 0.2175$		155.3	51.28	162.2	53.96	163.9	54.07	
		211.9	51.74	225.6	54.20	225.6	54.47	
		284.0	52.02	278.8	54.56	285.7	54.65	
	50.0	37.0	48.25	40.4	50.55	43.1	50.47	
		112.4	48.51	103.8	50.82	102.1	50.87	
		160.5	48.79	160.5	51.11	160.5	51.13	
		222.2	49.06	227.4	51.35	217.1	51.43	
		282.2	49.36	278.8	51.66	287.4	51.75	
hexane (1) + decane (2) +	25.0	34.8	51.48	43.1	53.85	40.4	53.75	
hexadecane (3)		103.8	51.78	114.1	54.12	109.0	53.98	
$x_1 = 0.4293$		157.0	52.04	150.2	54.37	148.4	54.29	
$x_2 = 0.2518$		225.6	52.34	211.9	54.73	225.6	54.57	
$x_3 = 0.3189$		278.8	52.71	285.7	55.08	278.8	55.00	
	50.0	43.1	49.12	36.9	51.12	42.1	51.18	
		98.7	49.47	109.0	51.40	103.8	51.50	
		150.2	49.69	155.3	51.66	160.5	51.74	
		225.6	49.84	222.2	52.09	218.8	52.18	
		280.5	50.11	278.8	52.30	289.1	52.48	



Figure 3. Pressure effect on the interfacial tension of *n*-alkane + water systems at 50.0 °C: (\bigcirc) C₁₆; (\times) C₁₄; (\triangle) C₁₂; (\bullet) C₁₀; (+) C₈; (\bullet) C₆.

Typical salt effects on the interfacial tension of $n-C_8 + brine$ systems are depicted in Figure 5. The effect of NaCl on the interfacial tension is significant.

The effect of temperature on the interfacial tension of $n-C_8 + H_2O$ and $n-C_{16} + H_2O$ were studied in the temperature range (25 to 80 °C) at fixed pressures; the results are given in Table 7 and plotted in Figure 6.

 Table 5. Coefficients in Eq 1 for Twenty *n*-Alkane +

 Water/Brine Systems

	<i>t</i> =	= 25.0 °C	t = 50.0 °C			
system	$\frac{\alpha}{mN\boldsymbol{\cdot}m^{-1}}$	$\frac{\gamma \times 10^{3/}}{m N \boldsymbol{\cdot} m^{-1} \boldsymbol{\cdot} bar^{-1}}$	$\frac{\alpha}{mN\cdot m^{-1}}$	$\gamma imes 10^{3/}$ mN·m ⁻¹ ·bar ⁻¹		
$\begin{array}{c} C_6 + H_2O\\ C_8 + H_2O \end{array}$	50.56 50.89	3.883 4.544	47.84 48.14	3.947 3.947		
$C_{10} + H_2O$ $C_{12} + H_2O$	51.32 51.84	4.836 5.401	48.86 49.21	4.431 5.112		
$C_{14} + H_2O$ $C_{16} + H_2O$ $C_{16} + hring 1$	52.18 52.67	5.446 5.415 4.018	49.80 50.16	5.252 5.946		
$C_6 + brine 1$ $C_6 + brine 2$ $C_8 + brine 1$	53.00 53.05 53.32	4.018 4.334 4.456	50.08 50.37 50.67	4.138 4.650 4.606		
$C_8 + brine 3$ $C_8 + brine 4$	51.66 52.54	3.797 5.154				
C ₈ + brine 5 C ₈ + brine 6	$55.90 \\ 53.36$	4.225 4.855				
C_8 + brine 7 C_{10} + brine 1	53.59 53.52	3.957 4.604	50.79	5.122		
C_{10} + brine 2 C_{12} + brine 1 C_{14} + brine 1	53.52 53.95 54 38	4.825 5.079 5.571	51.06 51.27 51.86	4.208 5.334 5.317		
C_{16} + brine 1 C_{16} + brine 2	54.85 54.92	5.807 5.187	52.47 52.44	5.644 5.866		

Conclusions

The following conclusions can be drawn from this study: The interfacial tension of n-alkane + water/brine systems increases slightly with pressure, and an approximately linear relationship is observed. The presence of salt in the aqueous phase increases the interfacial

Table 6. Comparison of Calculated (Based on Eq 1) and Literature Reported Data^{*a*} (mN·m⁻¹) for Four *n*-Alkane + Water Systems at 25.0 °C

	P = 5	0 bar	P = 1	00 bar	P=1	50 bar	P = 2	00 bar	P=2	50 bar
system	$\sigma_{\rm cal}$	σ_{exp}	$\sigma_{\rm cal}$	σ_{exp}	$\sigma_{\rm cal}$	$\sigma_{\rm exp}$	$\sigma_{\rm cal}$	σ_{exp}	$\sigma_{\rm cal}$	σ_{exp}
$C_6 + H_2O$	50.8	50.5	50.9	50.6	51.1	50.7	51.3	50.7	51.5	50.8
$C_8 + H_2O$	51.1	51.2	51.3	51.3	51.6	51.4	51.8	51.5	52.0	51.6
$C_{10} + H_2O$	51.6	51.6	51.8	51.7	52.0	52.0	52.3	52.1	52.5	52.2
$C_{12} + H_2O$	52.1	52.1	52.4	52.3	52.7	52.5	53.0	52.6	53.1	52.7

^a Experimental data read from the curves in Motomura et al. (1983).



Figure 4. Pressure effect on the interfacial tension of *n*-alkane + brine 1 systems at 50.0 °C: (\bigcirc) C₁₆; (\times) C₁₄; (\triangle) C₁₂; (\bullet) C₁₀; (+) C₈; (\bullet) C₆.



Figure 5. Salt effect on the interfacial tension of octane + brine systems at 25.0 °C: (\bigcirc) brine 5; (\times) brine 1; (\triangle) brine 4; (\bullet) brine 3; (+) H₂O.

tension. The increase depends on the concentration of the salt but is not sensitive to the salt species. The interfacial tension increases slightly with an increase in the molecular weight of the *n*-alkane.

Acknowledgment

Li-Min Zhang of the C. E. Class 90 has participated in partial experimental work.

Table 7.	Temperature Effects on the Interfacial Tension	ı
of <i>n</i> -C ₈ +	H ₂ O and <i>n</i> -C ₁₆ + H ₂ O Systems	

	$n-C_8 + 1$	H ₂ O	$n-C_{16} + H_2O$					
P/bar	t/°C	$\sigma/mN \cdot m^{-1}$	P/bar	t/°C	$\sigma/mN\cdot m^{-1}$			
40.4	25.0	51.73	36.9	25.0	52.91			
	37.0	49.92		50.0	50.31			
	46.0	48.81		60.0	49.37			
	50.0	48.33		70.0	48.75			
	58.0	47.20		80.0	47.66			



Figure 6. Temperature effect on the interfacial tension of octane + water (at 40.4 bar) and hexadecane + water (at 30.9 bar) systems: (\bigcirc) C₈; (\bullet) C₁₆.

Literature Cited

- Cai, B.-Y. A Study on the Interfacial Tension of n-Alkane-Water/Brine Systems under High Pressures. M.S. thesis, University of Petroleum, Beijing, P. R. China, 1995.
- Jennings, H. Y., Jr. The Effect of Temperature and Pressure on the Interfacial Tension of Benzene-Water and Normal Decane-Water. J. Colloid and Interface Sci. **1967**, 24, 323–329.
- Matubayasi, N.; Motomura, K.; Kaneshina, S.; Nakamura, M.; Matuura, R. Effect of Pressure on Interfacial Tension between Oil and Water. *Bull. Chem. Soc. Jpn.* **1977**, *50*, 523–524.
- McCaffery, F. G. Measurement of Interfacial Tensions and Contact angles at High Temperature and Pressure. J. Can. Petrol. 1972 (July-Sept), 26–32.
- Motomura, K.; Iyota, H.; Aratono, M.; Yamanaka, M.; Matuura, R. Thermodynamic Consideration of the Pressure Dependence of Interfacial Tension. J. Colloid Interface Sci. 1983, 93, 264-269.
- Nakahara, S.; Masamoto, H.; Arai, Y. Interfacial Tension of Two-Phase Water-Alkene Binary Liquid System. *J. Chem. Eng. Jpn.* **1990**, *23*, 94–95.
- Sada, E.; Kito, S.; Yamashita, M. Interfacial Tensions of Two-Phase Ternary Systems. J. Chem. Eng. Data 1975, 20, 376–377.

Received for review October 17, 1995. Accepted January 21, 1996. $^{\circ}$ Financial support received from the China National Petroleum & Natural Gas Corp. is gratefully acknowledged.

JE950259A

[®] Abstract published in Advance ACS Abstracts, March 15, 1996.